

**B.TECH SEM – VIII (2007 COURSE) (CHEMICAL ENGG.)  
: WINTER - 2017**

**SUBJECT: PROCESS EQUIPMENT DESIGN**

Day : **Thursday**  
Date : **23/11/2017**

**W-2017-2647**

Time : **02.30 PM TO 05.30 PM**  
Max. Marks : **80**

**N. B. :**

- 1) **Q. No. 1 and Q. No. 5 are COMPULSORY.** Out of remaining, attempt **ANY TWO** questions from each section.
- 2) Figures to the right indicate **FULL** marks.
- 3) Answers to both the sections should be written in **SEPARATE** answer books.
- 4) Draw neat and labeled diagrams **WHEREVER** necessary.
- 5) Use of non programmable calculator is allowed.
- 6) Assume suitable data, if necessary.

**SECTION – I**

- Q. 1**
- a) Draw schematic of H.E. showing all details of sheer side tube side, channels, gasket, flanges, inlets and outlet. **(05)**
  - b) What are different types of heating and cooling arrangements provided to chemical reactor? **(05)**
  - c) How does power requirement vary with laminar and turbulent region in agitator? **(04)**

- Q. 2** 5000 kg/hr of methanol vapours at two atm to be condensed by cooling water available at 10,000 kg/hr, 28<sup>0</sup>C. Assuming heat transfer coefficient on methanol vapor side to be 4,500 Wm<sup>2</sup>k. Find overall heat transfer coefficient, shell diameter giving tube pitch, baffle spacing? **(13)**  
Available pipe ID is 16 mm, 20 mm OD with 16 ft. length.  
U = 600W/m<sup>2</sup>

Methanol	P (atm)	1	2	3	4	5
	T ( <sup>0</sup> C)	64	78	34	92	99

- Q. 3** Six blade pitch blade turbine to be used to make fluorspar slurry in water @ 50<sup>0</sup>C. Viscosity of solution is 4 Pa.s, sp. gr.2.05. Diameter of vassel is 1.88 m. Agitator would be run at 20, 80, 200 rpm. **(13)**
- i) Find out power requirement for all three speeds.
  - ii) Suggest best rpm to operate with, logical reasoning.
  - iii) If above system has to be used for mixing fluid of 4 C<sub>p</sub> viscosity and sp. gr. of 1.4. What would be power requirement? If agitator turns @ 120 rpm.

**P. T. O.**

**Q.4** Biodiesel to be produced in a reactor with plain jacket for heating of reactor content. Suggest efficient design of shell jacket using following data: **(13)**

Reactor pressure	=	$5.56 \times 10^5 \text{ N/m}^2$
Jacket pressure	=	$3.56 \times 10^5 \text{ N/m}^2$
Jacket length	=	2.55 m
Temperature	=	145°C
Jacket internal diameter	=	2.27 m
Vessel shell internal diameter	=	2.14 m
Poisson's ratio	=	0.31
Modulus of elasticity	=	192 kN/m <sup>2</sup>
Allow stress for moe	=	99 N/m <sup>2</sup>

#### SECTION - II

**Q.5 a)** Draw schematic of compressor knockout drums. State its design for temperature and pressure. **(05)**

**b)** Draw schematic of actual distillation column with down comer, feed, distillate and bottom product outlet. Draw graph showing operating window for distillation. **(05)**

**c)** State safety devices in chemical industry. **(04)**

**Q.6 a)** Methanol-water 50 % (mole) mixture to be separated into distillation column to get 95 % (mole) methanol in top product leaving 5 % (mole) methanol in bottom product. If relative volatility is 1.9. How many numbers of plates would be sufficient for said separation, if column is operated at total reflux? **(07)**

**b)** How heat and mass transfer on every plate achieve purification as unit in distillation column? Explain with schematic and equation on every plate. **(06)**

**Q.7 a)** Crude oil is to be separated from water coming from oil well using decanter. Oil is in dispersed phase while water is in continuous phase. Oil flowrate is 0.278 kg/sec., sp. gr. Oil 0.9, oil viscosity 3 mNs/m<sup>2</sup>. Water flowrate is 83.33 kg/min, sp. gr. = 1, viscosity = 1 mNs/m<sup>2</sup>. Droplet diameter = 150 μm. **(09)**

What would be diameter of decanter, residence time of droplet, velocity of oil phase and entrained droplet size.

**b)** Describe any one gas liquid separator. **(04)**

**Q.8. a)** How do you find time required for drying in rotary dryer? State with mathematical expression. **(05)**

**b)** Ammonia + air mixture obtain from fertilizer plant is to be passed through packed tower with counter water flow. Gas inlet contains 11.2 % NH<sub>3</sub>, 99 % of NH<sub>3</sub> recovery is expected. equilibrium relation is :

$$Y = 15.4 X$$

$$Y = \frac{\text{kg } NH_3}{\text{kg air}} \quad X = \frac{\text{kg } NH_3}{\text{kg water}}$$

Water to gas rate is kept 30 % more than minimum value. What should be height of tower? (HTU)<sub>OG</sub> can be assumed 1 meter.

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