

**B.Tech Sem - VI (2007 Course) (Chemical Engg.) : WINTER - 2018**

**SUBJECT : CHEMICAL REACTION ENGINEERING – I**

Day : Wednesday  
Date : 14/11/2018

**W-2018-2838**

Time : 10.00 AM TO 01.00 PM  
Max. Marks : 80

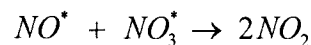
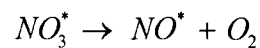
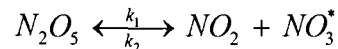
**N. B. :**

- 1) **Q. No.1 and Q. No. 5 are COMPULSORY.** Out of remaining attempt **ANY TWO** questions from section – I and section – II.
- 2) Figures to the right indicate **FULL** marks.
- 3) Answers to both the sections should be written in **SEPARATE** answer books.
- 4) Use of non-programmable calculator is **ALLOWED**.
- 5) Assume suitable data, if necessary.

**SECTION - I**

- Q. 1**
- a) Explain in detail and temperature dependency from Arrhenius law. **(05)**
  - b) Differentiate between integral method of analysis of data and differentiate method of analysis of data. **(05)**
  - c) Derive the performance equation of ideal batch reactor. **(04)**

- Q. 2** a) Show that the following scheme: **(06)**



is consistent with, and can explain, the observed first order decomposition of  $N_2O_5$ .

- b) For the stiochiometry  $A + B \rightarrow$  (Products) find the reaction orders with respect to A and B. **(07)**

i)

CA	4	1	1
CB	1	1	8
-rA	2	1	4

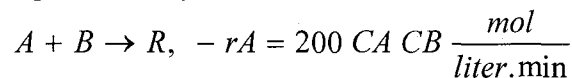
ii)

CA	2	2	3
CB	125	64	64
-rA	50	32	48

- Q. 3** a) After 8 minutes in a batch reactor reactant ( $CA_0 = 1 \text{ mol / litre}$ ) is 80 % converted after 18 minutes, conversion is 90 %. Find a rate equation to represent this reaction. **(06)**

- b) A 10 – minute experimental run shows that 75 % of liquid reactant is converted to product by a 1/2 order rate. What would be the fraction converted in a half hour run. **(07)**

- Q. 4** An aqueous feed of A and B (400 liter / min, 100 mmol A / liter, 200 mmol B / liter) is to be converted product in a PFR. The kinetics of the reaction is represented by **(13)**



Find the volume of the reactor needed for 99.9 % conversion of A to product.

**P. T. O.**

SECTION - II

Q. 5 a) Write a short note on autocatalytic reactions. (05)

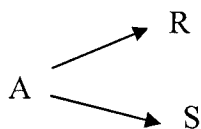
b) Explain in detail quantitative treatment of irreversible first order elementary reaction in PFR. (05)

c) Explain in detail adiabatic operations in PFR. (04)

Q. 6 a) At present conversion is 2/3 for our elementary second order liquid reaction  $2A \rightarrow 2R$  When operating in an isothermal plug flow reactor with a recycle ratio of unity. What will be the conversion if the recycle stream is shut off? (06)

b) 100 liters/hr of radioactive fluid having a half life of 20 hr. is to be treated by passing it through two stirred tanks in series,  $V = 40,000$  liters each. In passing through this system, how much will the activity decay? (07)

Q. 7 Liquid reactant A decomposes as follows. (13)



$$r_R = K_1 CA^2$$

$$r_S = K_2 CA$$

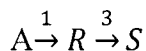
$$K_1 = 0.4 \text{ m}^3 / \text{mol} - \text{min}$$

$$k_2 = 2 \text{ min}^{-1}$$

A feed of aqueous A  $\left( CA_0 = 40 \frac{\text{mol}}{\text{m}^3} \right)$

enters a reactor, decomposes, and a mixture of A, R and S leaves. Find  $C_R$  and  $C_S$  and  $\tau$  for  $X_A = 0.9$  in a mixed flow reactor.

Q. 8 The first order reactions: (13)



S is desired.

$$K_1 = 10^9 e^{-6000/T}$$

$$K_2 = 10^7 e^{-4000/T}$$

$$K_3 = 10^8 e^{-9000/T}$$

$$K_4 = 10^{12} e^{-12,000/T}$$

are to be run in two MFR in series anywhere between  $10^0\text{C}$  and  $90^0\text{C}$ . If the reactors may be kept at different temperatures, what should these temperatures be for maximum fractional yield of S? Find this fractional yield.

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