

**M. TECH. -I (CHEMICAL ENGINEERING) (CBCS – 2015  
COURSE) : SUMMER - 2018**

**SUBJECT: ADVANCED MOMENTUM AND HEAT TRANSFER**

Day : **Wednesday**  
Date : **30/05/2018**

**S-2018-2991**

Time: **11.00 AM TO 02.00 PM**  
Max. Marks: 60.

**N.B.:**

- 1) All questions are **COMPULSORY**.
- 2) Figures to the **RIGHT** indicate full marks.
- 3) Both the sections should be written in **SEPARATE** answer books.
- 4) Draw neat diagrams **WHEREVER** necessary.
- 5) Assume suitable data, if necessary.

**SECTION-I**

- Q.1** Consider a flow of two adjacent immiscible fluids. These fluids are flowing in the z-direction in a horizontal thin slit of length L and width W under the influence of horizontal pressure gradient  $(P_0 - P_L)/L$ . The fluid flow rates are adjusted so that the slit is half filled with fluid I (more dense) and half filled with fluid II (less dense phase). Set up a differential momentum balance and obtain the expressions for momentum flux and velocity distribution. **(10)**

**OR**

A Newtonian fluid is in laminar flow in a narrow slit formed by two parallel walls a distance 2B apart. It is understood that  $B \ll W$ , so that edge effects are unimportant. Make a differential momentum balance and obtain the following expressions: **(10)**

$$\tau_{xz} = \left[ \frac{P_0 - P_L}{L} \right] x$$
$$v_z = \frac{(P_0 - P_L) B^2}{2\mu L} \left[ 1 - \left( \frac{x}{B} \right)^2 \right]$$

- Q.2** Predict the vortex depth in an agitated vessel. Consider two tanks with mechanical agitators. Large tank can be marked as 1 and small tank as 2. Derive the following expression. **(10)**

$$\gamma_2 = \gamma_1 \left[ \frac{D_2}{D_1} \right]^{1.5}$$

where,

$D_1$  and  $D_2$  – diameter of the two tanks.

$\gamma_1$  and  $\gamma_2$  – Kinematic viscosity of two liquids.

**OR**

Derive the equation of motion: **(10)**

$$\rho \frac{Dv}{Dt} = -\nabla P - (\nabla \cdot \tau) + \rho g$$

- Q.3** Show that for laminar flow in a thin slit of width 2B the friction factor is **(10)**

$$f = \frac{12}{Re} \text{ if } Re = \frac{2B \langle v \rangle \delta}{\mu} \text{ and}$$

$$v_z = \frac{(P_0 - P_L)}{2\mu L} B^2 \left[ 1 - \left( \frac{x}{B} \right)^2 \right]$$

**OR**

**P.T.O.**

Define friction factor for the packed column and derive - (10)

- a) Blake – Kozeny equation
- b) Burke – Plummer equation
- c) Ergun equation

**Q.4 a)** Explain the temperature and pressure dependence on thermal conductivity of liquids and solids. (05)

**b)** A plastic panel of area 1 ft<sup>2</sup> and thickness 0.252 inch was found to conduct heat at a rate of 3 watts at a steady state temperature of T<sub>0</sub>=24°C and T<sub>1</sub>=26 °C on two main surfaces. Determine the thermal conductivity. (05)

**OR**

For free convection between two vertical plates at two different temperatures, obtain an expression for velocity distribution as (10)

$$v_z = \frac{(\rho g \beta \Delta T) B^2}{12\mu} \left[ \left( \frac{y}{B} \right)^3 - \left( \frac{y}{B} \right) \right].$$

**Q.5 a)** Discuss the time smoothed temperature profile near a wall. Describe various regions based on the temperature profile. (05)

**b)** State the equation of motion for forced and free convection. (05)

**OR**

A solid slab occupying the space between  $y = -b$  and  $y = +b$  is initially at temperature T<sub>0</sub>. At time  $t = 0$  the surfaces at  $y = \pm b$  are suddenly raised to temperature T<sub>1</sub> and maintained at that temperature. Find T(y, t) for heating of this finite slab. (10)

**Q.6** Define heat transfer coefficient, the Nusselt number, the Stanton number and the Chilton – Colburn factor jH. Discuss in detail any one analogy for heat and momentum transfer. (10)

**OR**

What is the importance of analogies in transport phenomena? Explain in detail the Reynolds and Chilton–Colburn analogy between momentum and heat transfer. (10)

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